

5 **SOLUBLE, ASSOCIATIVE CARBOXYMETHYLCELLULOSE,
METHOD OF MAKING, AND USES THEREOF**

FIELD OF INVENTION

10 The present invention relates to water-soluble carboxymethylcelluloses (CMCs) that exhibit unique and highly desirable rheology and performance in end use systems and to a process for the preparation thereof. The CMCs of the present invention exhibit associative behavior both in neat solutions and in filled systems. The association is shear reversible, which enhances utility.

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BACKGROUND OF THE INVENTION

 Carboxymethylcellulose (CMC) is one of the most versatile and widely used cellulose ethers as a component for aqueous systems. It may act as a suspending agent, thickening agent, protective colloid, humectant, and for the control of crystallization of some other components. CMC is physiologically inert and is an anionic polyelectrolyte. The above noted characteristics makes CMC suitable for use in a wide spectrum of applications in the food, pharmaceutical, personal care, paper, building materials and construction, oilfield, and other industries.

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 There are many types of commercial CMCs available varying with respect to average degree of polymerization and substitution. The chemical and physical properties of the CMCs depend not only on the average degree of polymerization and substitution, but also on the overall solubility of the CMC as well as the distribution of carbomethoxy substituents along the cellulose chains. Both smoothly and blocky substituted CMCs are well known in the art. Blocky CMCs can be produced by lowering DS and/or changing the manufacturing process. However, processes that target a blocky CMC produce CMCs with limited solubility. In many cases a substantial portion of the CMC forms a swollen gel in aqueous applications. Such gels are undesirable in many applications, such as toothpaste, where the gel structure imparts an undesirable gel appearance in the toothpaste.

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US Patent Re 32,976 discloses a smoothly substituted, enzyme and salt resistant CMC which is prepared using an etherification agent which comprises at least 50% isopropyl monochloroacetate. Smoothly substituted CMCs will not provide the associative properties of the current invention. The CMCs of the present invention are prepared from monochloroacetic acid or sodium chloroacetate, not isopropyl monochloroacetate.

US Patent No. 4,579,943 discloses a CMC that has high liquid absorbing property that is derived from regenerated cellulose, having cellulose II form. The CMCs are of relatively low DS (0.1-0.64) and are substantially insoluble in water. The CMCs of the current invention are derived from cellulose I, not cellulose II or regenerated cellulose.

Publication WO 99/20657 discloses a CMC that has a tan delta of less than 1.0 at a concentration of 0.5 % under specific testing conditions. The CMC of the current invention do not have a tan delta less than 1.0 at 0.5% concentration.

The publication by G. Mann, J. Kunze, F. Loth and H-P fink of Fraunhofer Institut fur Angewandte Polymerforschung entitled "Cellulose ethers with a Block-like Distribution of the Substituents by Structure-selective Derivatization of Cellulose", Polymer, vol. 39, No. 14, pp. 3155-3165, Published 1998, discloses the preparation and testing of block-like distribution of CMC. The CMC is prepared by a step-by-step etherification reaction where a systematic carboxymethylation in alcohol-water medium is conducted while maintaining a low NaOH concentration (NaOH/AGU molar ratio < 0.6). The alkali cellulose is formed at elevated temperatures (50 – 70° C). It is reported that this process produces block-like cellulose ethers, including CMC, or cellulose etheresters with alternating hydrophilic and hydrophobic as well as various ionic chain segments. The CMCs are swollen particles in water and are not substantially soluble. The CMCs of the present invention are produced at higher NaOH/AGU ratios (about 1.1 to about 1.9) and low alkali cellulose temperatures (20 – 30° C), and are substantially soluble in water.

There is still a need for an associative, thixotropic CMC that exhibits associative behavior both in neat solutions and in filled systems. The association would be shear reversible, which would enhance utility. Such rheology would provide high thickening efficiency, and stabilize emulsions and suspensions, yet allow processing advantages such as ease of pumping or spreading, due to the reversible shear thinning characteristics of the associative network.

10 SUMMARY OF THE INVENTION

The present invention is related to a composition comprising CMC having a relative urea/water ratio of less than about 0.9. The relative urea ratio is defined as:

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$$\begin{aligned}
 \text{Relative Viscosity in 6M Urea} &= \frac{\text{Dynamic Viscosity of 1\% CMC in 6M urea}}{\text{6M urea viscosity}} = \frac{\text{Dynamic Viscosity of 1\% CMC in 6M urea}}{1.4 \text{ cP}} \\
 \text{Relative Viscosity in Water} &= \frac{\text{Dynamic Viscosity of 1\% CMC in Water}}{\text{Water viscosity}} = \frac{\text{Dynamic Viscosity of 1\% CMC in 6M urea}}{0.89 \text{ cP}} \\
 \text{Relative Urea/Water Ratio} &= \frac{\text{Relative Viscosity in 6M Urea}}{\text{Relative Viscosity in Water}}
 \end{aligned}$$

This invention is also directed to a process for making a CMC comprising a) reacting in an aqueous slurry of isopropyl alcohol, a source of cellulose, and about 50 – 80% of the stoichiometric level of alkali for a sufficient time and at a sufficient temperature to form an alkali cellulose b) adding sufficient alkali to bring the total alkali concentration to stoichiometric levels, followed by addition of the requisite amount of etherification agent, c) completing the etherification reaction and optionally, d) adjusting final molecular weight/viscosity by addition of oxidizing agents capable of degrading cellulosic chains.

This invention also comprehends the use of the CMC of the present invention in an aqueous rheology modifier system as a vehicle component of a

personal care, household care, paint, building material, construction, pharmaceutical, oilfield, food, paper making or paper coating composition.

BRIEF DESCRIPTION OF DRAWINGS

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Figure 1 shows a graph of toothpaste viscosity over time.

Figure 2 shows a graph of toothpaste viscosity overtime that has been normalized.

Figure 3 shows a graph of toothpaste structure over time.

10 Figure 4 shows a graph of toothpaste structure over time that has been normalized.

Figure 5 shows a graph of crushing strengths of blends of polymers.

Figure 6 shows a graph of percent drug dissolved over time.

Figure 7 shows a graph of percent drug dissolved over time.

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DETAILED DESCRIPTION OF THE INVENTION

A CMC has been surprisingly discovered that exhibits unique and highly desirable rheology and performance properties in end use systems.

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In accordance with the present invention, the viscosity builds up not only by means conventional to CMC, but also is boosted significantly by molecular association. The association leads to network formation and gel-like rheological properties. The fact that the association is shear reversible enhances utility.

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The CMCs of the present invention have been shown to lower the CMC use level needed and to provide rheology attributes unique from other CMCs available today. The unique rheology provides high thickening efficiency, and stabilizes emulsions and suspensions. The CMCs of the present invention
30 provide significantly enhanced performance over known CMCs in aqueous systems including personal care formulations (e.g., toothpaste, skin care, and hair care), medical care (e.g., wound care and ostomy), food applications (i.e., tortillas, cake mixes, bread mixes, bread, ice cream, sour cream, pasteurized processed cheese spreads, and cheese foods), beverages (i.e., instant cold/hot

drinks, ready to drink beverages, and fruit flavored drinks), paint systems, building and construction materials (such as joint formulations), mineral processing, oil field formulations (e.g., drilling fluids), paper making and paper coating formulations, household formulations (e.g., laundry detergents, fabric softeners), and pharmaceutical formulations.

In accordance with the present invention, when the composition is a personal care composition, it includes (a) from about 0.1 % to about 99.0 % by weight of the vehicle component and (b) at least one active personal care ingredient. Examples of the at least one active personal care ingredient are deodorant, skin coolants, emollients, antiperspirant actives, moisturizing agents, cleansing agents, sunscreen actives, hair treatment agents, oral care agents, tissue paper products, and beauty aids.

In accordance with the present invention, the composition is a household care composition, it includes (a) from about 0.1 % to about 99.0 % by weight of the vehicle component and (b) at least one active household care ingredient. Examples of the at least one active household care ingredient are industrial grade bar, gel and liquid soap actives, all purpose cleaning agents, disinfecting ingredient, rug and upholstery cleaning actives, laundry softeners actives, laundry detergent ingredients, dishwashing detergents, toilet bowl cleaning agents and fabric sizing agents.

In addition to the ingredients conventionally used in the personal care and household care, the composition according to the present invention can optionally also include ingredients such as a colorant, preservative, antioxidant, nutritional supplements, activity enhancer, emulsifiers, viscosifying agents (such as salts, i.e., NaCl, NH₄Cl & KCl, water-soluble polymers, i.e., hydroxyethylcellulose, and fatty alcohols, i.e., cetyl alcohol), alcohols having 1-6 carbons, and fats and oils.

The CMCs may also be used in combination with other known rheology modifiers including, but not limited to, polysaccharides (e.g., carrageenan, guar, hyaluronic acid, glucosaminoglycan, hydroxyethyl cellulose, hydrophobically

modified hydroxyethyl cellulose, ethyl hydroxyethyl cellulose, hydroxypropyl methylcellulose, hydroxyethyl methylcellulose, methylcellulose, cationic guar, carbomer), biopolymers (e.g., xanthan), synthetic polymers (polyethylene glycol, polyvinylacetate, chlorohexidiene), and thickening silicas.

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The use of CMC in toothpaste formulations is well known in the toothpaste industry as a binder system for toothpaste that gives the toothpaste a desirable high structure. The binder system includes CMC types with other polysaccharides, inorganic salts, chelating agents and combinations thereof.

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Commercially available CMC types vary in the degree of structure they provide to the toothpaste. Highly thixotropic grades of CMC tend to render toothpaste of higher structure. These thixotropic CMC types also tend to contribute to greater post-thickening.

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Cellulose gum (CMC) alone has been a traditional binder for toothpaste. In toothpaste, CMC provides viscosity, stand-up or structure, and syneresis control. Toothpaste made with CMC is also known to have a slow rate in viscosity build up over the shelf life of the toothpaste thus not reaching a stable viscosity until after first 30 days or more. This is also called "post-thickening".

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Other binders commonly used in toothpaste are carrageenan or carrageenan and xanthan together. Carrageenan and xanthan provide good stand-up, viscosity and syneresis control; however, they tend to be more expensive alternatives as compared to CMC. Toothpaste made with carrageenan and xanthan tend to exhibit a stable viscosity rather quickly after processing and little post-thickening.

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In accordance with the present invention, the CMC of the present invention can be use either alone or in combination with other polysaccharides, synthetic polymers and or salts and provide high efficiencies and enhanced performance. See the toothpaste Examples hereinafter for the demonstration of the unexpected results of the present invention.

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Use of the CMCs of the present invention have allowed a use level reduction of about 40% while maintaining critical toothpaste properties such as stand-up, gloss and syneresis control. The lower use levels and/or shear thinning behavior of the CMCs may offer additional advantages to toothpaste properties such as improved flavor release, improved actives delivery, improved fluoride delivery, higher gloss, improved extrudability from the tube, and improved anti-microbial effectiveness. Potential improvements to the toothpaste manufacturing process include, but are not limited to, reduction of entrapped air during manufacturing process, improvements in mixing operations, and improvements in extrusion into tubes.

Water-based protective coating compositions (commonly referred to as paints) in which cellulose ether derivatives are conventionally used include latex paints or dispersion paints, of which the principal ingredients are film-forming lattices such as styrenebutadiene copolymers, vinyl acetate polymers and copolymers, and acrylic polymers and copolymers. Typically, they also contain opacifying pigments, dispersing agents and water-soluble protective colloids, the proportions being, by weight of the total composition, about 10 parts to about 50 parts of a latex, about 10 parts to about 50 parts of an opacifying pigment, about 0.1 part to about 2 parts of a dispersing agent, and about 0.1 part to about 2 parts of a water-soluble protective colloid.

Water soluble protective colloids conventionally used in the manufacture of latex paints (to stabilize the lattices and maintain the wet edge of a painted area longer in use) include casein, methyl cellulose, hydroxyethylcellulose (HEC), sodium carboxymethyl cellulose (CMC), polyvinyl alcohol, starch, and sodium polyacrylate. The disadvantages of the natural based cellulose ethers are that they may be susceptible to biological degradation and frequently impart poor flow and leveling properties, while the synthetic materials such as polyvinyl alcohol often lack enough thickening efficiency to maintain sag resistance. The thickening efficiency of the cellulose ethers is usually improved by increasing their molecular weight which normally is more expensive.

In accordance with the present invention, the CMC of the present invention can be used in lower amounts in paints and provide unexpected high quality results. This is illustrated in the working Examples hereinafter.

5 The CMCs of the present invention are prepared using conventional slurry process methods. For example, isopropyl alcohol, water, and about 50 –80% of the stoichiometric amount of NaOH are reacted with cellulose at a temperature of about 20°C for a sufficient time to produce alkali cellulose, about 1.5 hours. Sufficient NaOH is added to bring the total NaOH level to or slightly above
10 stoichiometric levels and monochloroacetic acid is added shortly after the second NaOH addition. The reaction conditions are normally to raise the temperature to about 70°C for about one to two hours to effect etherification. The molecular weight and viscosity of the CMC can be adjusted (reduced) by addition of an oxidizing agent, such as hydrogen peroxide, subsequent to
15 etherification. The reaction mass is then optionally cooled, excess base neutralized, if necessary, and the product is washed. This product can then be dried and ground. The critical feature of this invention is that the amount of alkali utilized to effect etherification is less than stoichiometric and that the remaining alkali is added just prior to the etherification agent. The degree of substitution of
20 the CMC is about 0.6 to about 1.2.

In accordance with the present invention, the CMC can be differentiated from prior art CMCs by their being substantially soluble in aqueous media environments and their behavior in environments that do not favor association. It
25 is a known fact that urea breaks up association by breaking hydrogen bonds. The subject CMCs exhibit a viscosity decrease in the presence of urea, as determined by the relative urea ratio. The relative urea ratio is defined as:

$$\begin{aligned}
 \text{Relative Viscosity in 6M Urea} &= \frac{\text{Dynamic Viscosity of 1\% CMC in 6M urea}}{\text{6M urea viscosity}} = \frac{\text{Dynamic Viscosity of 1\% CMC in 6M urea}}{1.4 \text{ cP}} \\
 \text{Relative Viscosity in Water} &= \frac{\text{Dynamic Viscosity of 1\% CMC in Water}}{\text{Water viscosity}} = \frac{\text{Dynamic Viscosity of 1\% CMC in 6M urea}}{0.89 \text{ cP}} \\
 \text{Relative Urea/Water Ratio} &= \frac{\text{Relative Viscosity in 6M Urea}}{\text{Relative Viscosity in Water}}
 \end{aligned}$$

EXAMPLES

The following examples are merely set forth for illustrative purposes, but it is to be understood that other modifications of the present invention within the skill of an artisan in the related industry can be made without departing from the spirit and scope of the invention. All percentages and parts are by weight unless specifically stated otherwise.

Example 1

Isopropyl alcohol (IPA, 696.67g) and deionized (DI) water (76.945g) were charged into a jacketed resin kettle reactor equipped with an air driven stirrer, stainless steel agitator, a pressure equalizing addition funnel, a reflux condenser, vacuum, nitrogen inlet and a thermocouple. A cellulose pulp (65.0g, 6.4% moisture) was added to the reactor, the reactor was sealed, and the agitator was adjusted to obtain good mixing. The reactor was inerted and the mixture was cooled to 20°C.

Aqueous NaOH (50%, 60.92g) was slowly added to the reactor through the addition funnel, maintaining the mixture slurry temperature at 20°C. The reaction mixture was held for 1 hour at 20°C after the caustic addition was completed.

Aqueous NaOH (50%, 16.02g) was slowly added to the reactor through the addition funnel, maintaining the mixture slurry temperature at 20°C. The reaction mixture was held for 5 minutes at 20°C after the caustic addition was completed. Monochloroacetic acid (MCA, 42.91g) was added to the reactor through an open reactor port, maintaining a reactor slurry temperature of 20°C. After MCA addition was completed, the reaction slurry was heated to 70°C and held for 1.5 hours. The reaction slurry was filtered and the resulting wet cake was washed three times with 565g of 80% aqueous methanol and one time with 1000g of pure methanol. The resulting wet cake was broken into small particles and dried in a fluidized bed dryer for 35 minutes. (Air-dry for 5 minutes, heat-dry at 50°C for 10 minutes, and heat-dry at 70°C for an additional 20 minutes.) The

product was ground in Retsch Grinding Mill using a 1mm screen. Degree of Substitution (DS) = 0.89

Example 2

5 Isopropyl alcohol (IPA, 696.67g) and deionized (DI) water (76.945g) were charged into a jacketed resin kettle reactor equipped with an air driven stirrer, stainless steel agitator, a pressure equalizing addition funnel, a reflux condenser, vacuum, nitrogen inlet and a thermocouple. A cellulose pulp (65.0g, 6.4% moisture) was added to the reactor, the reactor was sealed, and the agitator was
10 adjusted to obtain good mixing. The reactor was inerted and the mixture was cooled to 20°C.

Aqueous NaOH (50%, 60.92g) was slowly added to the reactor through the addition funnel, maintaining the mixture slurry temperature at 20°C. The
15 reaction mixture was held for 1 hour at 20°C after the caustic addition was completed.

Aqueous NaOH (50%, 16.02g) was slowly added to the reactor through the addition funnel, maintaining the mixture slurry temperature at 20°C. The
20 reaction mixture was held for 5 minutes at 20°C after the caustic addition was completed. Monochloroacetic acid (MCA, 42.91g) was added to the reactor through an open reactor port, maintaining a reactor slurry temperature of 20°C. After MCA addition was completed, the reaction slurry was heated to 70°C and held for 1.5 hours. 1.6 ml of 6% H₂O₂ was added to the reactor and the slurry
25 was heated at 70°C for 30 minutes. The reaction slurry was filtered and the resulting wet cake was washed three times with 565g of 80% aqueous methanol and one time with 1000g of pure methanol. The resulting wet cake was broken into small particles and dried in a fluidized bed dryer for 35 minutes. (Air-dry for 5 minutes, heat-dry at 50°C for 10 minutes, and heat-dry at 70°C for an
30 additional 20 minutes.) The product was ground in Retsch Grinding Mill using a 1mm screen. Degree of Substitution (DS) = 0.87.

Example 3

Isopropyl alcohol (IPA, 123.4 gallons), water (130.3 lbs), methanol (6.36 gallons), and NaOH (flake, 35.4 lbs.) were charged into the reactor. The reactor was inerted and the caustic/solvent mix was cooled to about 20°C, at which time
5 a cellulose pulp (108lbs, 4% moisture) was added to the reactor. The agitation was adjusted to give good mixing in the slurry and the slurry was recooled to about 20°C. The reaction slurry was held for 1 hour at 20°C.

Aqueous NaOH (50%, 58.7 lbs.) was added to the reactor and the
10 reaction mixture was held for 15 minutes at 20°C after the caustic addition was completed. Monochloroacetic acid (MCA, 70.5 lbs.). IPA (9.0 gallons), dichloroacetic acid (DCA, 926.8g) and acetic acid (79.9g) were added to the reactor, maintaining a reactor slurry temperature of 20°C. After MCA addition was completed, the reaction slurry was heated to 70°C and held for 1 hour. 282g
15 of 18% H₂O₂ was added to the reactor and the slurry was heated at 70°C for 60 minutes.

The reaction slurry was centrifuged and the wet cake was washed with three times with 300 gallons of 80% methanol and two times with 300 gallons
20 100% methanol. The material was dried in an Abbe dryer under vacuum at 80 – 90°C to a moisture content of 4 – 6 %. The product was ground in a micropulverizer through a 0.0278 inch screen. Degree of Substitution (DS) = 0.79.

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Example 4

The conditions of Example 3 were repeated. DS = 0.78

Example 5

Isopropyl alcohol (IPA, 121.9 gallons), water (130.0 lbs), methanol (6.29
30 gallons), and NaOH (flake 45.6 lbs.) were charged into the reactor. The reactor was inerted and the caustic/solvent mix was cooled to about 20°C, at which time a cellulose pulp (108lbs, 4% moisture) was added to the reactor. The agitation was adjusted to give good mixing in the slurry and the slurry was recooled to about 20°C. The reaction slurry was held for 1 hour at 20°C.

Aqueous NaOH (50%, 58.7 lbs.) was added to the reactor and the reaction mixture was held for 15 minutes at 20°C after the caustic addition was completed. Monochloroacetic acid (MCA, 81.0 lbs.). IPA (9.0 gallons), dichloroacetic acid (DCA, 1065.9g) and acetic acid (91.9g) were added to the reactor, maintaining a reactor slurry temperature of 20°C. After MCA addition was completed, the reaction slurry was heated to 70°C and held for 1 hour. 188g of 18% H₂O₂ was added to the reactor and the slurry was heated at 70°C for 60 minutes.

The reaction slurry was centrifuged and the wet cake was washed with three times with 300 gallons of 80% methanol and two times with 300 gallons 100% methanol. The material was dried in an Abbe dryer under vacuum at 80 – 90°C to a moisture content of 4 – 6 %. The product was ground in a micropulverizer through a 0.0278 inch screen. Degree of Substitution (DS) = 0.86.

Example 6

The conditions of Example 5 were repeated. DS = 0.86

Example 7

Isopropyl alcohol (IPA, 121.1 gallons), water (146.0 lbs), methanol (6.24 gallons), and NaOH (flake, 35.4 lbs.) were charged into the reactor. The reactor was inerted and the caustic/solvent mix was cooled to about 20°C, at which time a cellulose pulp (108lbs, 4% moisture) was added to the reactor. The agitation was adjusted to give good mixing in the slurry and the slurry was recooled to about 20°C. The reaction slurry was held for 1 hour at 20°C.

Aqueous NaOH (50%, 58.7 lbs.) was added to the reactor and the reaction mixture was held for 15 minutes at 20°C after the caustic addition was completed. Monochloroacetic acid (MCA, 70.5 lbs.). IPA (9.0 gallons), dichloroacetic acid (DCA, 926.8g) and acetic acid (79.9g) were added to the reactor, maintaining a reactor slurry temperature of 20°C. After MCA addition was completed, the reaction slurry was heated to 70°C and held for 1 hour. 282g

of 18% H₂O₂ was added to the reactor and the slurry was heated at 70°C for 60 minutes.

The reaction slurry was centrifuged and the wet cake was washed with three times with 300 gallons of 80% methanol and two times with 300 gallons 100% methanol. The material was dried in an Abbe dryer under vacuum at 80 – 90°C to a moisture content of 4 – 6%. The product was ground in a micropulverizer through a 0.0278 inch screen. Degree of Substitution (DS) = 0.79.

Example 8

Isopropyl alcohol (IPA, 14 kg), water (2184g), methanol (728.8g), were charged into the reactor. The reactor was inerted and the solvent mix was cooled to about 20°C, at which time a cellulose pulp (1800 g, 3.6% moisture) was added to the reactor. The agitation was adjusted to give good mixing in the slurry, the slurry was recooled to about 20°C, and NaOH (flake, 691.4g) was added to the reactor. The reaction slurry was held for 1 hour at 20°C.

Aqueous NaOH (50%, 353.6g) was added to the reactor and the reaction mixture was held for 15 minutes at 20°C after the caustic addition was completed. Monochloroacetic acid (MCA, 939.8g). IPA (977g), dichloroacetic acid (DCA, 27.3g) and acetic acid (2.4g) were added to the reactor, maintaining a reactor slurry temperature of 20°C. After MCA addition was completed, the reaction slurry was heated to 70°C and held for 1 hour.

The reaction slurry was filtered, and the resulting wet cake was washed three times with 12 gallons of 80% aqueous methanol, and one time with 12 gallons of 95% methanol. The material was dried in a vacuum tray dryer at 70°C to a final moisture content of 4 – 6%. The dried product was ground in a micropulverizer through a 0.0278 inch screen. Degree of Substitution = 0.73.

Example 9

Isopropyl alcohol (IPA, 696.67g) and deionized (DI) water (76.95g) were charged into a jacketed resin kettle reactor equipped with an air driven stirrer,

stainless steel agitator, a pressure equalizing addition funnel, a reflux condenser, vacuum, nitrogen inlet and a thermocouple. A cellulose pulp (65.0g, 6.8% moisture) was added to the reactor, the reactor was sealed, and the agitator was adjusted to obtain good mixing. The reactor was inerted and the mixture was cooled to 20°C.

Aqueous NaOH (50%, 60.92g) was slowly added to the reactor through the addition funnel, maintaining the mixture slurry temperature at 20°C. The reaction mixture was held for 1 hour at 20°C after the caustic addition was completed.

Aqueous NaOH (50%, 36.37g) was slowly added to the reactor through the addition funnel, maintaining the mixture slurry temperature at 20°C. The reaction mixture was held for 5 minutes at 20°C after the caustic addition was completed. Monochloroacetic acid (MCA, 42.91g) was added to the reactor through an open reactor port, maintaining a reactor slurry temperature of 20°C. After MCA addition was completed, the reaction slurry was heated to 70°C and held for 1.5 hours. 1.6 ml of 6% H₂O₂ was added to the reactor and the slurry was heated at 70°C for 30 minutes. The reaction slurry was filtered and the resulting wet cake was washed three times with 565g of 80% aqueous methanol and one time with 1000g of pure methanol. The resulting wet cake was broken into small particles and dried in a fluidized bed dryer for 35 minutes. (Air-dry for 5 minutes, heat-dry at 50°C for 10 minutes, and heat-dry at 70°C for an additional 20 minutes.) The product was ground in Retsch Grinding Mill using a 1mm screen. Degree of Substitution (DS) = 0.62. 1% aqueous viscosity = 2200 cps.

Example 10

Isopropyl alcohol (IPA, 713.86g) and deionized (DI) water (73.79g) were charged into a jacketed resin kettle reactor equipped with an air driven stirrer, stainless steel agitator, a pressure equalizing addition funnel, a reflux condenser, vacuum, nitrogen inlet and a thermocouple. A cellulose pulp (65.0g, 3.7% moisture) was added to the reactor, the reactor was sealed, and the agitator was

adjusted to obtain good mixing. The reactor was inerted and the mixture was cooled to 20°C.

Aqueous NaOH (50%, 39.98g) was slowly added to the reactor through the addition funnel, maintaining the mixture slurry temperature at 20°C. The reaction mixture was held for 1 hour at 20°C after the caustic addition was completed.

Aqueous NaOH (50%, 35.77g) was slowly added to the reactor through the addition funnel, maintaining the mixture slurry temperature at 20°C. The reaction mixture was held for 5 minutes at 20°C after the caustic addition was completed. Monochloroacetic acid (MCA, 42.25g) was added to the reactor through an open reactor port, maintaining a reactor slurry temperature of 20°C. After MCA addition was completed, the reaction slurry was heated to 70°C and held for 1.5 hours. The reaction slurry was filtered and the resulting wet cake was washed three times with 565g of 80% aqueous methanol and one time with 1000g of pure methanol. The resulting wet cake was broken into small particles and dried in a fluidized bed dryer for 35 minutes. (Air-dry for 5 minutes, heat-dry at 50°C for 10 minutes, and heat-dry at 70°C for an additional 20 minutes.) The product was ground in Retsch Grinding Mill using a 1mm screen. Degree of Substitution (DS) = 0.84. 1% aqueous viscosity = 3760 cps.

Example 11

This Example illustrates the behavior of the preparations of a 1.0% CMC samples of the present invention in a 6.0 M urea solution.

The 1 % CMC solution was prepared in the following equipment:

Caframo RZR1 overhead stirrer, 8-oz. glass jars, stainless steel stirring shaft with two 3-blade propellers (1.5 inch diameter), Parafilm®, deionized (DI) water, Germaben II.

A 0.50% Germaben solution was prepared by adding the Germaben II to DI water. This solution was then weighed into an 8-oz. glass jar. The solution was then stirred with an overhead stirrer, while the CMC was quickly added to

the solution. The CMC level is 1.0% of the final sample weight. CMC weight is corrected for moisture content. As the viscosity begins to increase, the speed of the stirrer was increased to the maximum rate that does not cause splashing out of the sample. The jar is covered with Parafilm while mixing to prevent evaporation of water and loss from splashing. The sample is stirred for one hour. After one hour of stirring at the highest rate, the stirring speed was decreased to a setting of 4 for one additional hour. The sample was centrifuged for approximately 5 minutes to remove trapped air.

The behavior of the samples were studied in the following equipment:
Caframo RZR1 overhead stirrer, 8-oz. glass jars, stainless steel stirring shaft with two 3-blade propeller (1" diameter), Parafilm®, 6.0M Urea (180.18g urea diluted to 500ml)

Procedure:

6.0M urea solution was weighed into an 8-oz. glass jar. The solution was stirred with an overhead Caframo RZR1 stirrer, as the CMC was quickly added to the solution. The CMC level was 1.0% of the final sample weight. CMC weight was corrected for moisture content. As the viscosity begins to increase, the speed of the stirrer was increased to the maximum rate that does not cause splashing out of the sample. The jar was covered with Parafilm while mixing to prevent evaporation of water and loss from splashing. The sample was stirred for one hour. After one hour of stirring at the highest rate, the stirring speed was decreased to a setting of 4 for one additional hour. The sample was centrifuged for approximately 5 minutes to remove trapped air.

Table 1

CMC	DS	1% Dynamic Water viscosity	1% Dynamic 6M Urea viscosity	R _{lativ} U/W ratio
Example 8	0.73	1113	1364	0.78
Example 1	0.89	574	632	0.70
Example 2	0.87	238	288	0.77
Example 7	0.79	762	539	0.45
Example 5	0.86	265	338	0.81
Example 3	0.79	286	355	0.79
Example 4	0.78	346	398	0.73
Example 6	0.86	163	228	0.89
Aqualon 7LF	0.81	11	16	0.97
Aqualon 7LF		11	17	0.96
Aqualon 7L	0.79	9	14	0.97
Aqualon 7H3SF	0.97	7191	12754	1.13
Aqualon 7H3SF	0.92	2286	4179	1.16
Aqualon 7H3SF	0.88	7337	13258	1.15
Aqualon 7H3XSf	0.89	3262	5909	1.15
Aqualon 7H3SXf		3111	4950	1.01
Aqualon 7HF	0.86	7023	11648	1.05
Aqualon 7H4F	0.77	4875	8576	1.12
Aqualon 7M8SF		68	111	1.03
Aqualon 9M31F	0.9	260	467	1.14
Aqualon 9M31F	0.92	577	1065	1.17
Aqualon 9M31F	0.9	539	823	0.97
Aqualon 9M31XF		282	470	1.06
Amtex		168	282	1.07
Antisol FL 300000		2852	8510	1.90
Aqualon Aquapac		7795	12583	1.03
Aqualon Aquapac		11446	19881	1.10
DKS Cellogen HE-90		100	179	1.14
DKS Cellogen HP-5HS		4417	8154	1.17
Fine Gum SA-H		463	1016	1.40
Monpac Regular		2755	5980	1.38
Noviant Cekol 500T		47	68	0.92
Noviant Cekol 700		53	96	1.16
Noviant Cekol 2000		139	246	1.13
PAC-R		7335	11798	1.02
Tylopur C1000 P2		316	558	1.12
Walocel CRT 2000		180	285	1.01

The flavor was mixed in the same way. After all formula components were together, the mixture was mixed under vacuum for 15 minutes at high speed. The batch was then packed into 2-oz. jars and 6-oz. toothpaste tubes.

- 5 Toothpaste samples were stored for 30 days at room temperature. Samples were equilibrated in a 25°C water bath for 4 hours prior to any tests conducted.

10 Viscosity was measured using a Brookfield DV-I fitted with a T-bar style spindle. A helipath stand was used to allow the spindle to sweep downward through the sample to prevent the effects of shear. Viscosity was taken every 30 seconds over 2 minutes and values were averaged.

15 Toothpaste consistency was measured using a rack test. The rack designed with cross bars of increasing distance apart left to right. The toothpaste tube containing the sample to be measured is fitted with a stainless orifice fitting to eliminate differences in orifice size that may occur. The tube is squeezed in a uniform manner across the rack, extruding the paste onto the rack in a ribbon. After 15 seconds it is recorded at which opening the ribbon has
20 fallen through the opening and broken. The opening number from left to right is the value recorded as a "Cuban" value.

The toothpaste data are summarized in Table 2.

25

Table 2

Polymer	30 day Toothpaste Viscosity	Cuban	Comments
Example 2	137500	5	
Example 1	188125	10	
Example 3	146750	6	
Example 4	136250	6	
Example 5	120000	5	
Example 6	94500	3	
Example 7	125750	5	
Cekol 500T	61875	2	
Cekol 2000	25875	0	severe syneresis
9M31XFGL	40125	0	syneresis
9M31F	32500	0	syneresis

Example 14

The CMC's of the present invention in combination with other polymers exhibit decreased post thickening and structure build and enhanced initial structure in toothpaste formulations.

Viscosity is one measure of post-thickening in toothpaste. Toothpaste samples were packed into vials and the viscosity was measured using a Brookfield DV-I fitted with a T-bar style spindle. A helipath stand was used to allow the spindle to sweep downward through the sample to prevent the effects of shear. Viscosity was taken every 30 seconds over 2 minutes and values were averaged

It can be seen from the data in the graph (Figure 1) that most samples exhibited a change in viscosity from the first day after processing through 30 days. When the data are normalized to the initial viscosity as 100%, the change over time is more apparent (Figure 2). Toothpaste made with combinations of Example 7 CMC with other polysaccharides or inorganic salts exhibited lower post-thickening compared to toothpaste made with Example 7 alone.

Toothpaste structure is also an important aspect. This property may be measured by force required for compression using a MTS Servo Hydraulic test system from MTS Systems Corporation, Minneapolis, MN. The instrument was fitted with a half-inch acrylic cylinder probe, toothpaste samples were packed into vials after processing and measured directly without disturbance.

It can be seen below in Table 3 that the Example 7 CMC alone or with other polysaccharides or inorganic salt produced toothpaste of similar or greater initial structure compared to toothpaste made with carrageenan and xanthan and much greater initial structure than toothpaste made with commercial CMC 9M31F.

Peak force of compression was monitored over 30 days. It was found that most samples changed in values (Figure 3). The comparison can be made more

Exempl 12

Dynamic viscosities were measured using at 25°C using an RFS III strained controlled rheometer by Rheometrics using a 40 mm parallel tool geometry with the gap set at 2 mm. The samples were pre-sheared at 100s⁻¹ for 5 60 second upon loading to erase the loading history. The pre-shearing was followed by the steady shear experiment between 0.01 and 100s⁻¹. Each point data is the average of clockwise and counter-clockwise rotations each with the duration of 20 sec. All samples exhibited a low shear Newtonian plateau, the average of which was used in the data analysis and further comparisons. The 10 dynamic viscosities of the aqueous and 6M 1% CMC solutions are summarized in Table 1. The relative urea/water ratios are also summarized in Table 1, above.

Example 13

15 The CMC's of the present invention exhibit enhanced thickening capabilities and syneresis control in toothpaste formulations. Calcium Carbonate Based Toothpaste formulation:

Ingredient:	wt. %
Calcium carbonate	45.00
Sorbo® sorbitol (70% solids)	27.00
Distilled water	23.97
CMC Polymer (Table 2)	0.60
Sodium lauryl sulfate, 100% active powder	1.00
25 Sodium monofluorophosphate	0.76
Sodium benzoate	0.50
Flavor	0.55
Tetra sodium pyrophosphate	0.42
Sodium saccharin	<u>0.20</u>
30	100.00

Standard laboratory toothpaste preparation was performed. Salts were first dissolved in part of the water and warmed for complete dissolution. The CMC was dispersed in the sorbitol, using an overhead mixer with a propeller 35 attachment. After the CMC was well dispersed, the balance of the water was added with continued mixing until the CMC appeared dissolved. The warm salt solution was mixed into the CMC solution. This was then transferred to a 1-quart Ross double planetary mixer. The calcium carbonate was then stirred in the mixer, and after it was well dispersed, a vacuum was applied. After mixing under 40 vacuum for 20 minutes, the sodium lauryl sulfate was mixed in without vacuum.

easily if the data are normalized to the initial structure value as 100% as shown in Figure 4. From the normalized data of Figure 4, it can be seen that toothpaste samples made with combinations of CMC of Example 7 with other polysaccharides or inorganic salt have lower structure build over time.

5

From the work outlined here, it can be concluded that toothpaste with high structure and low post-thickening can be made with CMCs of the present invention in combination with other polysaccharides, inorganic salts or combinations thereof.

10

The toothpaste formulation used in this Example was as follows:

Ingredient	Wt. %
Sorbitol (Sorbo)	29.2
Glycerine	6
PEG 400	3
Sident 9	14
Sident 22S	16
Sodium Saccharine	0.20
Sodium Monofluorophosphate	0.23
Sodium Benzoate	0.20
Sodium Lauryl Sulfate	1.20
Flavor	0.50
Water	q.s.

15 The different polymers used in this Example in the formulation was as follows:

Formulation	Polymer:	wt%	Polymer:	wt%
1	Carrageenan (THP1)	0.7	Xanthan (Rhodicare)	0.3
2	CMC Example 7	1.0	N/A	
3	CMC 9M31F	1.0	N/A	
4	CMC Example 7	0.5	Natrosol + 330	0.3
5	CMC Example 7	0.6	Natrosol 250 M	0.6
6	CMC Example 7	0.7	Carrageenan	0.3
7	CMC Example 7	1.0	Sodium Silicate	0.5
8	CMC Example 7	0.7	Xanthan	0.3

Table 3

Initial Toothpaste Structure
Peak Force Compression from MTS

Polymer	Peak Force Compression, g
Carageenan/Xanthan	56.5
Example 7	51.1
Example 7 / HMHEC	78.1
Example 7 / Na ₂ SiO ₃	60.8
Example 7 / HEC	75.1
Example 7 / Carrageenan	75.3
Example 7 / Xanthan	35.0
CMC 9M31 F	14.7

Toothpaste after 24 hours, ambient temperature.

The identity and supplier of the ingredients of this Example are as follows:

Sorbitol	Sorbo, 70%, USP/FCC, SPI Pharma, New Castle, DE, USA
Glycerine	Glycerine, USP, Spectrum Chemical, Gardena, CA, USA
PEG 400	Polyethylene Glycol NF, Dow Chemical, Midland, MI, USA
Silica, thickening	Sident 9, Degussa, Frankfurt, Germany
Silica, abrasive	Sident 22S, Degussa, Frankfurt, Germany
Sodium Lauryl Sulfate	Stepan, Northfield, IL, USA
Flavor	Fresh Mint, Givaudan, UK
Sodium Silicate, crystalline	JT Baker, reagent grade
Sodium Benzoate	Fisher Scientific, reagent grade
Saccharine	Sigma, reagent grade
Sodium Fluorophosphate	Alfa Aesar, Ward Hill, ME, USA
Carrageenan	THP1, CP Kelco, San Diego, CA, USA
Xanthan	Rhodicare S, Rhodia, Cranbury NJ, USA
CMC 9M31F	Aqualon
HM HEC Natrosol Plus 330 CS	Aqualon
HEC Natrosol 250 M Pharm	Aqualon

Example 15

The CMC's of the present invention exhibit enhanced thickening capabilities in beverage formulations.

Beverage Example

Orange Beverage - Reference

Ingredients

	Wt %
Orange Juice concentrate, 45 Brix	7.00
Sugar	40.00
Citric acid	0.05
Sodium benzoate	0.55
Water	52.14
Cellulose Gum, CMC-9M31F	0.60

Orange Beverage - Test Example

	<u>Ingredients</u>	<u>Wt %</u>
	Orange Juice concentrate, 45 Brix	7.00
5	Sugar	40.00
	Citric acid	0.05
	Sodium benzoate	0.55
	Water	52.14
	Polymer Example 7	0.42

10

Mix cellulose gum or polymer into water, allow to mix for 20 minutes.

Premix acid, preservative and sugar, add and mix 5 minutes. Add juice concentrate, mix 3 minutes.

15	<u>Beverage results:</u>	<u>Reference</u>	<u>Test Example</u>
	Viscosity, 24 hours, cps	53.0	51.0
	Brookfield LV, spindle 2, 30 rpm, 20s		

20

Example 16

The CMC's of the present invention exhibit enhanced thickening capabilities in food formulations.

Cake Mix and Cake Example

25	CAKE MIX - Reference		
	<u>Ingredients for Dry Mix</u>	<u>% Flour wt</u>	<u>Wt % of dry mix</u>
	Bleached Cake Flour	100	40.4
	Sugar	105.9	42.2
	Shortening	27.2	11.0
30	Milk Solids Nonfat	3.7	1.5
	Dextrose ⁽¹⁾	2.5	1.0
	Salt	2.5	1.0
	Sodium Bicarbonate ⁽²⁾	2.2	0.9
	Sodium aluminum phosphate ⁽³⁾	1.2	0.9
35	Vanilla Powder ⁽⁴⁾	1.2	0.5
	Butter Flavor ⁽⁵⁾	0.3	0.1
	Cellulose Gum, CMC-7HF	1.2	0.5

CAKE MIX - Test Example

	<u>Ingredients for Dry Mix</u>	<u>% Flour wt</u>	<u>Wt % of dry mix</u>
	Bleached Cake Flour	100	40.4
5	Sugar	105.9	42.2
	Shortening	27.2	11.0
	Milk Solids Nonfat	3.7	1.5
	Dextrose ⁽¹⁾	2.5	1.0
	Salt	2.5	1.0
10	Sodium Bicarbonate ⁽²⁾	2.2	0.9
	Sodium aluminum phosphate ⁽³⁾	1.2	0.9
	Vanilla Powder ⁽⁴⁾	1.2	0.5
	Butter Flavor ⁽⁵⁾	0.3	0.1
	Polymer Example 9	0.72	0.3

- 15 (1) Arm & Hammer Baking Soda, Church & Dwight
(2) Cantab Dextrose, Penford Food Ingredient Company
(3) Levair, FCC Grade Sodium Aluminum Phosphate, Rhodia Food Ingredients
(4) Vanilla FL Pure Pwd K, Virginia Dare
(5) Butter FL N&A Pwd 685 KD, Virginia Dare

20

Formulation for the Finished Cake - One 8-inch Layer

	Dry mix, g	270
	Water, g	140
25	Whole egg, g	53

Dry ingredients were blended on mixer with paddle attachment until evenly mixed. Water and egg were added to mix and mixed on medium speed for 3 minutes. The batter was poured into a greased cake pan and baked in a moderate oven (350°F/177°C) for 30 minutes.

	<u>Cake results:</u>	<u>Reference</u>	<u>Test Example</u>
	Batter Viscosity, cps	5660	7650
	Brookfield RV, spindle 3, 10 rpm, 30 s		
35	Batter density, g/100mls	111	113
	Cake height, cm	3.8	3.8
	Crumb cell structure	even	even
	Bake out	OK	OK
	Crumb moisture, 24 hours after bake, %	39.0	39.0

40

Example 17

The CMCs of the present invention exhibit efficiency by the use of reduced amounts but yet obtain corporate results with prior art materials. The film forming and viscosity properties are enhanced in food preparations.

45

Masa and Corn Tortilla Example

MASA - Reference

	<u>Ingredients for Dry Mix</u>	<u>% Flour wt</u>	<u>Wt % of dry mix</u>
	NCF ⁽¹⁾	100	98.83
5	Sodium Benzoate	0.4	0.39
	Fumaric Acid	0.3	0.29
	Cellulose Gum, CMC-7H4F K	0.5	0.49

	<u>Ingredients for Dry Mix</u>	<u>% Flour wt</u>	<u>Wt % of dry mix</u>
10	NCF ⁽¹⁾	100	98.63
	Sodium Benzoate	0.4	0.39
	Fumaric Acid	0.3	0.29
	Polymer Example 10	0.3	0.29

15
(1)Nixtamalized corn flour, Quaker Oats Company

Dry ingredients were blended on mixer with paddle attachment until evenly mixed. Water was added to mix and mixed on medium speed for 2
20 minutes. Dough was portioned into 50g balls and pressed on a tortilla press. The tortillas were baked on an ungreased skillet for 1 minutes on each side. Tortillas were cooled on a wire rack, wrapped in foil sheets and checked for pliability and reheat after 1 day.

25	<u>Tortilla results:</u>	<u>Reference</u>	<u>Test Example</u>
	Appearance after bake	even blisters	even blisters
	Pliability	good roll, no cracks	good roll, no cracks
	Reheat	good puff	good puff

30

Example 18

The CMC's of the present invention exhibit enhanced tablet crushing strength without effecting drug release kinetics.

The following formulations were prepared:

	Total batch size	1500g
		3750 Tablets
Material	%	Wt per Tab (Mg)
Example 7	7.5	30
Klucel HXF	22.5	90
Phenylpropanolamine	20.0	80
Avicel PH101	49.5	198
Magnesium Stearate	0.5	2

	Total batch size	1500g
		3750 Tablets
Material	%	Wt per Tab (Mg)
Example 7	7.5	30
Natrosol 250 HX	22.5	90
Theophylline	20.0	80
Avicel PH101	49.5	198
Magnesium Stearate	0.5	2

5

	Total batch size	1500g
		3750 Tablets
Material	%	Wt per Tab (Mg)
CMC 12M8 PH	7.5	30
Klucel HXF	22.5	90
Phenylpropanolamine	20	80
Avicel PH101	49.5	198
Magnesium Stearate	0.5	2

	Total batch size	1500 g
		3750 Tablets
Material	%	Wt per Tab (Mg)
CMC 12M8 PH	7.5	30
Natrosol 250 HX	22.5	90
Theophylline	20	80
Avicel PH101	49.5	198
Magnesium Stearate	0.5	2

Experimental Procedures:

10

All ingredients were sieved through a 20 mesh screen. All ingredients except magnesium were then dry blended in a 4 quart low shear Hobart mixer for 2 minutes. Thereafter water was added at a rate of 100 g/min while using low speed stirring. A total of 500ml per 1500 g of powder was added to the

formulations containing Klucel. This was increased to 700g for Natrosol containing formulations. The wet masses were tray dried at 60°C down to less than 2 % moisture content. Following the drying step, the granulations were milled using the Fitzpatrick Comminutor Fitzmill at 2300 rpm, knives forward.

- 5 The reduced granulation was then lubricated by addition of 0,5% magnesium stearate. This final mix was blended for 3 minutes in a V-blender.

Compactibility:

- 10 As shown in Figure 5 for both model formulations, the inclusion of Example 7 CMC in place of CMC 12M8 pH in the tablet matrix results in a significant increase in tablet crushing strength.

Drug Release Kinetics

- 15 While compactibility is improved, inclusion of Example 7 CMC does not manifest in significant differences in the release kinetics when compared to 12M8 pH. This shown in figures 6 and 7 for both highly soluble drug (phenylpropanolamine) and a sparingly soluble drug (Theophylline). Additionally no differences were evident at pH 1.5 or 6.8 between the Example 7 CMC and
20 CMC 12M8 containing formulations.

Example 19

- The CMC's of the present invention exhibit enhanced thickening efficiency, enhanced high shear viscosity (ICI), improved spatter resistance and
25 improved water resistance in paint formulations.

Model of an interior latex flat paint based on Acronal 290 D.

Position	Ingredients	Function	Parts by weight
1.	Water		230.0
5 2.	Calgon N	wetting agent	1.5
3.	Pigmentverteiler A	dispersing agent	3.0
4.	CA 24	preservative	3.0
5.	Agitan 280	defoamer	5.0
6.	thickener	rheological modifier	variable
10 pre-mix			
7.	Kronos 2057	pigment	198.0
8.	Omyalite 90	extender	140.0
9.	Durcal 5	extender	198.0
10.	Talcom AT 200	extender	28.0
15 mill base			
11.	Acronal 290 D	latex binder	93.0
13.	butylglycol	coalescing agent	20.0
14.	Texanol		5.0
15.	additional water		71.5
20 let down			
PVC (%)	80%		
NVW (%)	61%		
25 Suppliers:			
2	Benckiser Knapsack GmbH		
3	BASF AG		
4	Biochema Schwaben – Dr. Lehmann & Co.		
5	Münzing Chemie GmbH		
30 6	Aqualon / HERCULES		
7	Kronos Titan GmbH		
8	Plüss Staufer SG		
9	Plüss Staufer SG		
10	a/s Norwegian Talc		
35 11	BASF AG		
12	Shell Nederland Chemie BV		
13	Eastman Chemicals		

Thickener	TE [wt. %]	Brookfield (20/4) 24 hrs [mPa.s]	Stormer Initial [KU]	Stormer 24 hrs [KU]	ICI [mPa.s]	Lovelling [Leneta]	Lovelling [NYPC]	Sag resistance [µm]	Spatter resistance	Water reten. ² [mm]
BLANOSE® 7M31C	0.57	7050	98	106	125	5	0	600	2-3	4
BLANOSE® 7M31C	0.48	6750	97	103	120	4	0	600	2-3	5
BLANOSE® 7M31C	0.45	6500	97	104	150	2	0	550	3	4
Example 7 CMC	0.41	7550	97	107	150	1	0	600	4	3

Rating

1)

0-10, 10 = BEST

2)

Water resistance test acc. Grimshaw; 0 mm = best

ICI Viscosity Determination: Determined using ASTM D4287-83

Krebs Stormer Viscosity Measurement: Determined using ASTM D 562

5 Levelling Leneta : Determined using ASTM D 4062-81

Levelling test NYPC: Determined using ASTM D 2801-69

Sag Resistance: Determined using ASTM D4400-84

10

Spatter Resistance – Roller:

The following equipment was used to evaluate the samples:

15

paint roller with synthetic fibers e.g. verroller 15 cm art.nr. 32913 ex Van
Vliet Kwastenfabriek

wall paper (woodchip quality) e.g. Erfurt Raufaser 52

20

Procedure:

About 200 grams of paint is taken up by the roller. Paint is applied on a
woodchip wallpaper with dimensions 100 x 50 cm placed in vertical position.

Paint is applied by ten- up and down strokes with the roller. A piece of black

25

carch paper is placed horizontally 50 cm below the bottom line of the wallpaper.

The amount of spatter that is intercepted on the black paper is compared to a
series of reference charts rating from 1 to 10. A rating of 1 means severe spatter
and a rating of 10 stands for completely spatter free.

30

Water Retention (According GRIMSHAW)

Equipment used in this part of the experment is:

Substrate: Whatman No. 1 circular

Filter paper (diameter 12.5 cm)

35

Clamp ring inner diameter 7.7 cm
outer diameter 12.6 cm

Pasteur pipette (poly ethylene disposable)

Colorant: Quink parket permanent block ink

40

Balance

Procedure

1. Mix a blend of paint/colorant thoroughly in an aluminum cup.
Depending on the viscosity the following ratio's can be chosen:
5 Paint: colorant 50:50
 60:40
 75:25
Total amount 4-5 grams
- 10 2. Put the filter paper between two clamp rings and fix these with paper clips.
3. Weigh the clamped filter paper and apply with a Pasteur pipette 0.5 or 1.0
gram (depending the fluidity of the colored point blob) on the center of the
filter paper.
- 15 4. Allow an overnight drying at room temperature.
5. Measure with a ruler the shaded stain round the paint center on 6 different
spots.
- 20 6. The average expressed in mm is a measure for the water retention. A low
value means a good water retention.
7. Report the used test conditions, ratio and amount of paint as well as the
25 increase of the stain in mm.

While this invention has been described with respect to specific
embodiments, it should be understood that these embodiments are not intended
to be limiting and that many variations and modifications are possible without
30 departing from the scope and spirit of this invention.